

# CBCS SCHEME - Make-Up Exam



BBT601

**Sixth Semester B.E/B.Tech. Degree Examination, June/July 2025**

## Bioprocess Control and Automation + Lab

Max. Marks:100

**Note:** 1. Answer any FIVE full questions, choosing ONE full question from each module.  
2. M : Marks , L: Bloom's level , C: Course outcomes.

Module – 1				M	L	C
1	a.	With neat diagram, explain the principle and working of i) Thermocouple and ii) RTD		10	L2	CO1
	b.	Describe the online methods for biomass estimation.		10	L2	CO1
OR						
2	a.	With a neat sketch, explain the working principle of i) Diaphragm gauge and ii) Bourdon tube		10	L2	CO1
	b.	Explain the measurement of physical and chemical parameters.		10	L2	CO1
Module – 2						
3	a.	Obtain the transfer function for liquid level single tank system.		12	L2	CO2
	b.	A thermometer having a time constant of 10 seconds is placed in a temperature batch. After the thermometer reaches steady state temperature of 30°C, it is suddenly placed into a hot fluid at 60°C, Sketch the response of the thermometer.		8	L3	CO2
OR						
4	a.	Obtain the sinusoidal response for the first order transfer function.		12	L2	CO2
	b.	A thermometer is observed to exhibit the first order dynamics having the time constant of 12 s and is placed in water bath. After the thermometer reaches steady state temperature of 30°C with the water bath, temperature of the bath is linearly increased with time at a rate of 6°C/ min Obtain the response for the thermometer at 5 sec, 10 sec and 15 sec. Determine the dynamic error and time lag of the system.		8	L3	CO2
Module – 3						
5	a.	Obtain the transfer function for three tank non interacting liquid level system.		10	L2	CO2
	b.	The overall T.F of the control system is given as $G(s) = \frac{16}{1.5s^2 + 2.4s + 6}$ A step change of magnitude 6 is introduced into the system. Determine : i) Overshoot ii) Period of Oscillation iii) Natural period of Oscillation iv) Rise time v) Ultimate Value of response vi) Maximum value of response		10	L3	CO2



OR

6	a.	Obtain the Transfer function for U – tube Manometer	10	L2	CO2
	b.	Derive a step response for the second order system.	10	L3	CO2

## Module – 4

7	a.	With a neat sketch, explain pneumatic control valve.	10	L2	CO3
	b.	Determine the overall transfer function $c(s) / R(s)$ for the system shown in figure.	10	L3	CO3

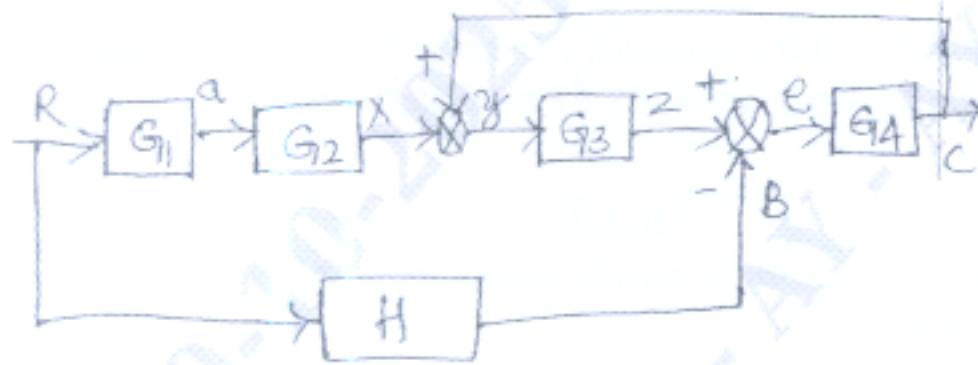


Fig. Q. 7(b)

OR

8	a.	Derive the transfer function for servo problem with neat block diagram.	12	L2	CO3
	b.	A unit step change is given to a PI controller. If the proportional sensitivity or gain ( $K_c$ ) is 4, integral time is 2, obtain the response of PI controller.	8	L3	CO3

## Module – 5

9	a.	Sketch the root locus diagram for the system, if the open loop T.F is $G(s) = \frac{K_c}{s(s+1)(s+2)}$	10	L4	CO4
	b.	Obtain the bode diagram for first order system.	10	L4	CO4

OR

10	a.	A PD controller having derivative time, $\tau_D = 4$ is used to control two non-interacting first order systems with $\tau_1 = 1$ and $\tau_2 = 0.5$ Gain of the system is 0.5. Determine the stability of the control system.	10	L4	CO4
	b.	The open loop transfer function of control system is given as $G(s) = \frac{K_c(0.5s+1)}{s(s+1)(s+0.5)}$ . Sketch the root locus diagram of the control system. Indicate the open loop poles, zero, break away point. Determine the value of gain of the controller $K_c$ for which the system becomes just unsalable.	10	L4	CO4

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